

# Lignocellulosic Biomass Valorisation using Deep Eutectic Solvents for Sustainable Biorefineries

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## INTRODUCTION

Lignocellulosic biomass (LBM) represents a renewable, widespread and low-cost source which can potentially be converted to fine chemicals and bio-fuels.

30-40% of the total production costs accounts for the feedstock cost.

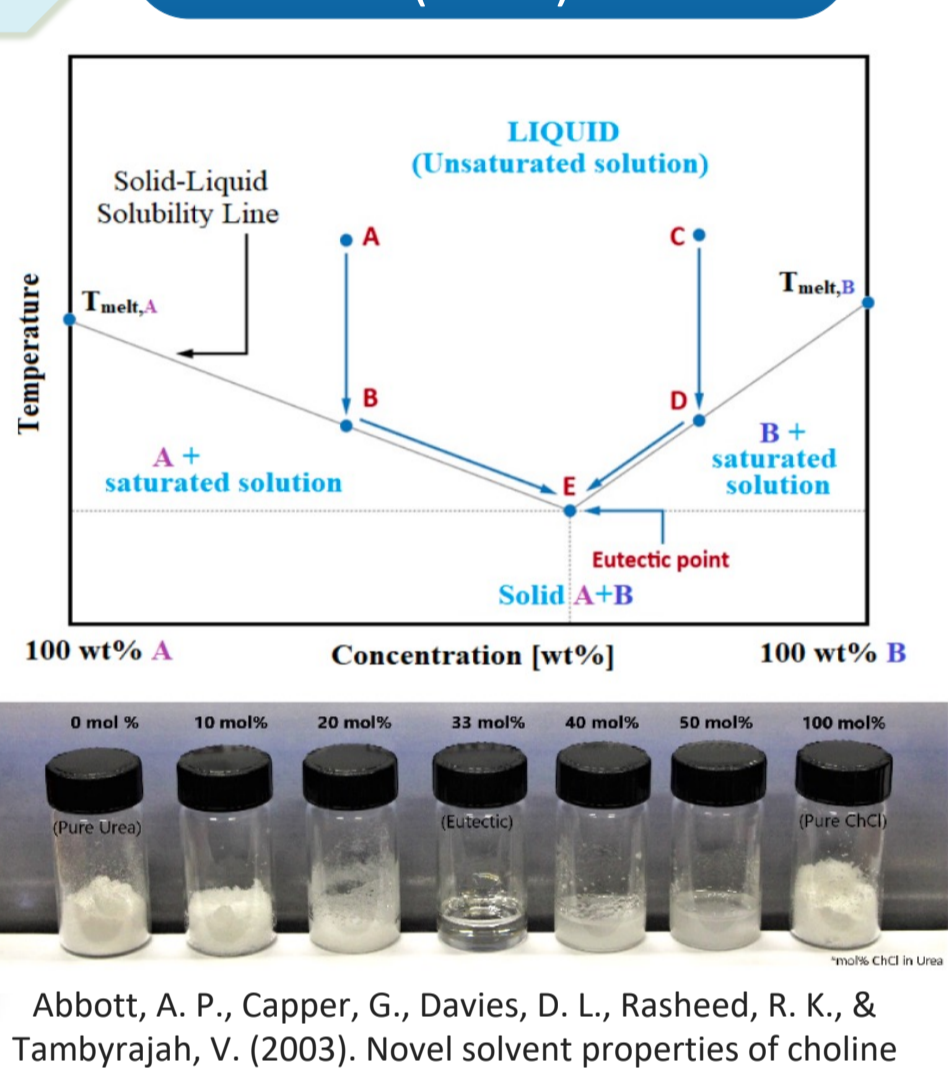
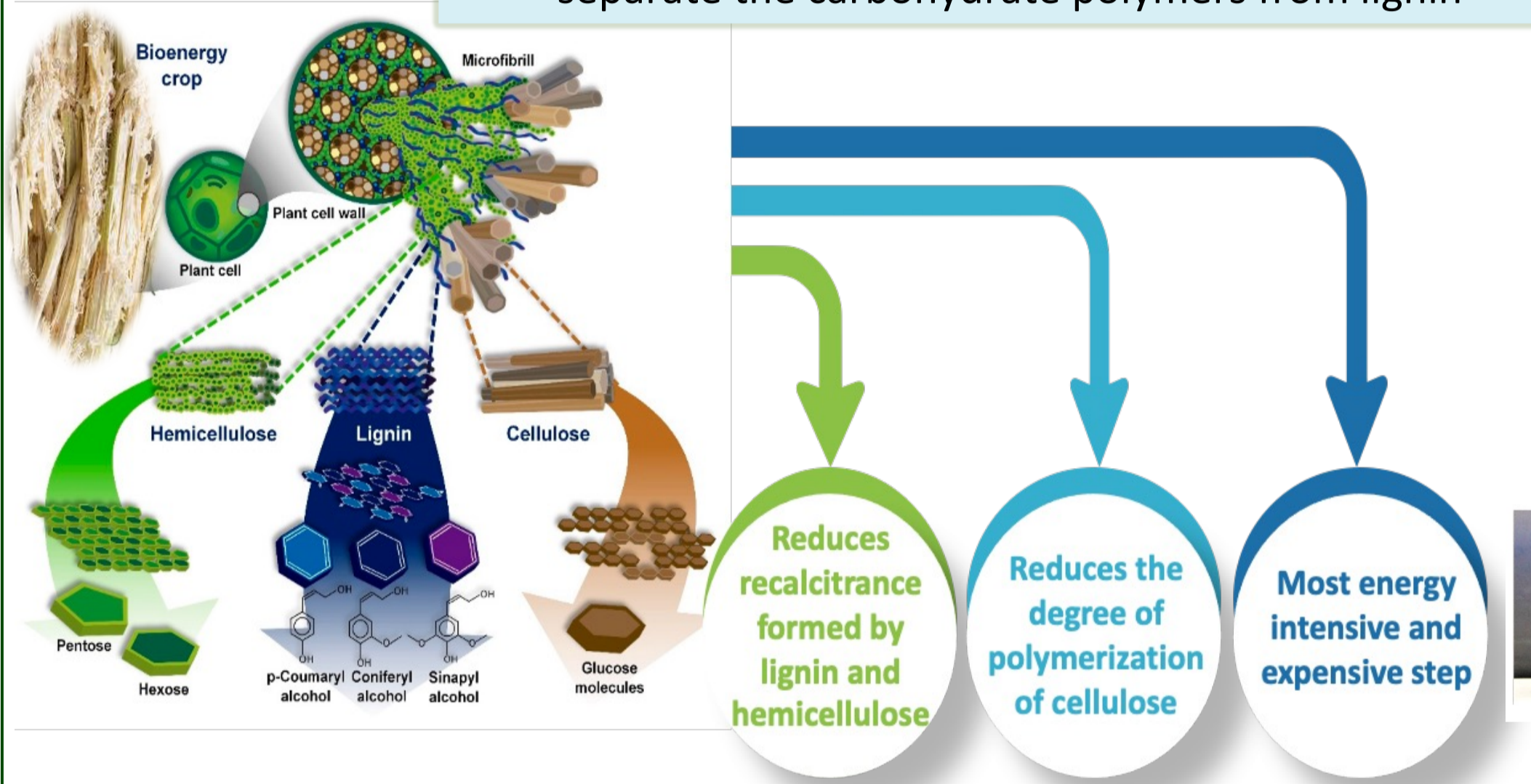


Sources of Agricultural residue	Annual production (million tons)
Barley Straw	51.3
Corn Stover/ Straw	376.8
Rice Straw	657.5
Wheat Straw	472.2
<b>Sugarcane Bagasse</b>	<b>1044.8</b>

Source: Y. Y. Tye et al. Renewable and Sustainable Energy Reviews 60 (2016) 155-172

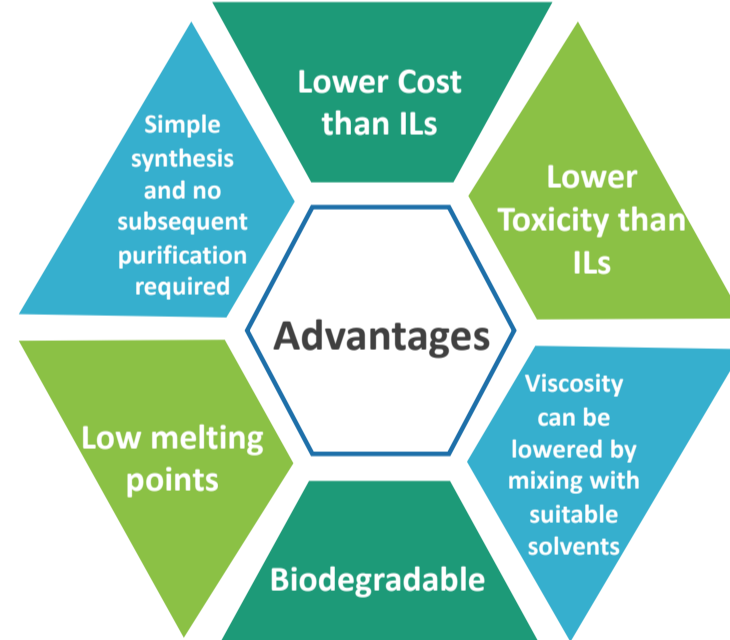
**Pre-treatment:** Process for depolymerising biomass to separate the carbohydrate polymers from lignin

**Deep Eutectic Solvents (DESs)**



Abbott, A. P., Capper, G., Davies, D. L., Rasheed, R. K., & Tambyrajah, V. (2003). Novel solvent properties of choline chloride/urea mixtures. *Chemical Communications*, (1), 70-71.

- DESs are greener alternatives to ionic liquids with identical properties.
- Melting points lower than that of the individual liquid.
- Consist of hydrogen bond acceptor (HBA), commonly a quaternary ammonium salt, complexed with a hydrogen bond donor (HBD) at appropriate molar ratios.



## MATERIALS AND METHODS

### Preparation of Sugarcane bagasse (SB)

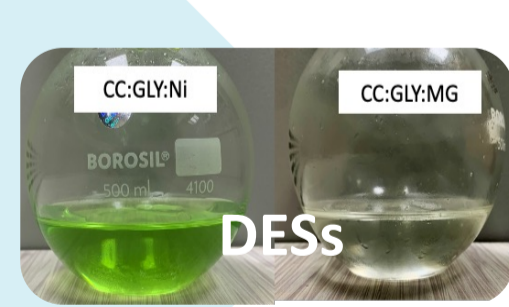


### Preparation of DESs

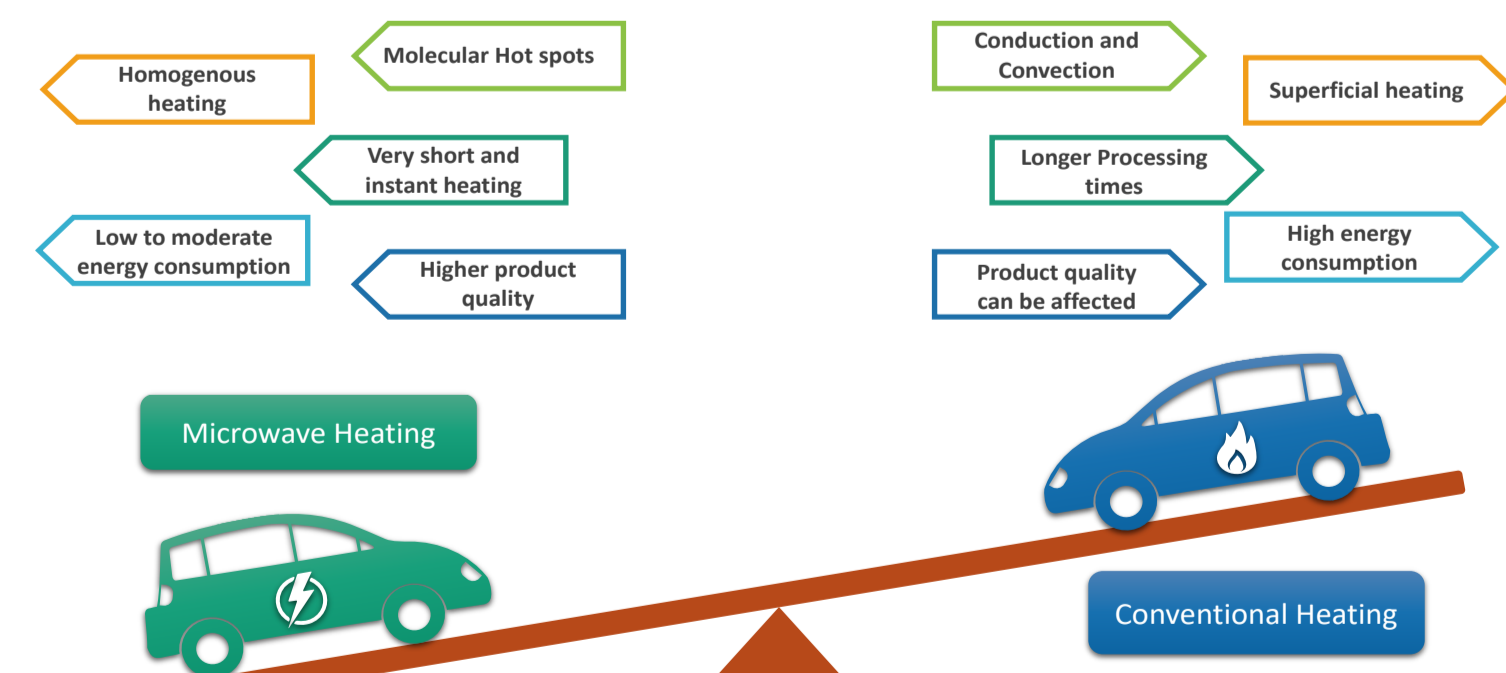
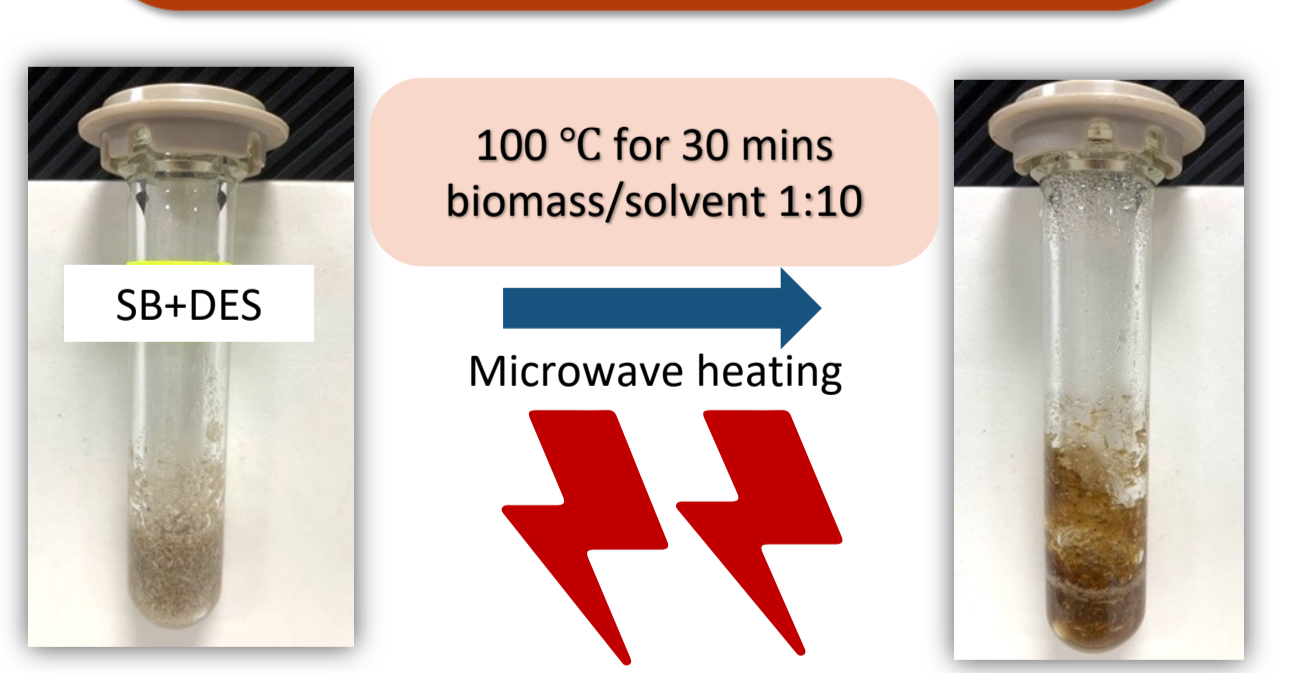
- DES Components (1:2:0.016)**
- Choline chloride : Ethylene Glycol:  $MgCl_2 \cdot 6H_2O$  (CC:EG:MG)
  - Choline chloride : Glycerol:  $MgCl_2 \cdot 6H_2O$  (CC:GLY:MG)
  - Choline chloride : Ethylene Glycol:  $NiCl_2 \cdot 6H_2O$  (CC:EG:NI)
  - Choline chloride : Glycerol:  $NiCl_2 \cdot 6H_2O$  (CC:GLY:NI)

### Process

Mixing with continuous stirring @ 70°C for 2h



### Microwave assisted Pre-treatment of SB using DESs



### One Pot Integrated Bioethanol Production

#### 1. DES Pre-treatment

- CC:EG:MG and CC:EG:NI
- Biomass : Solvent :: 1:10
- Conditions: 100 °C, 30 mins

#### 2. Saccharification

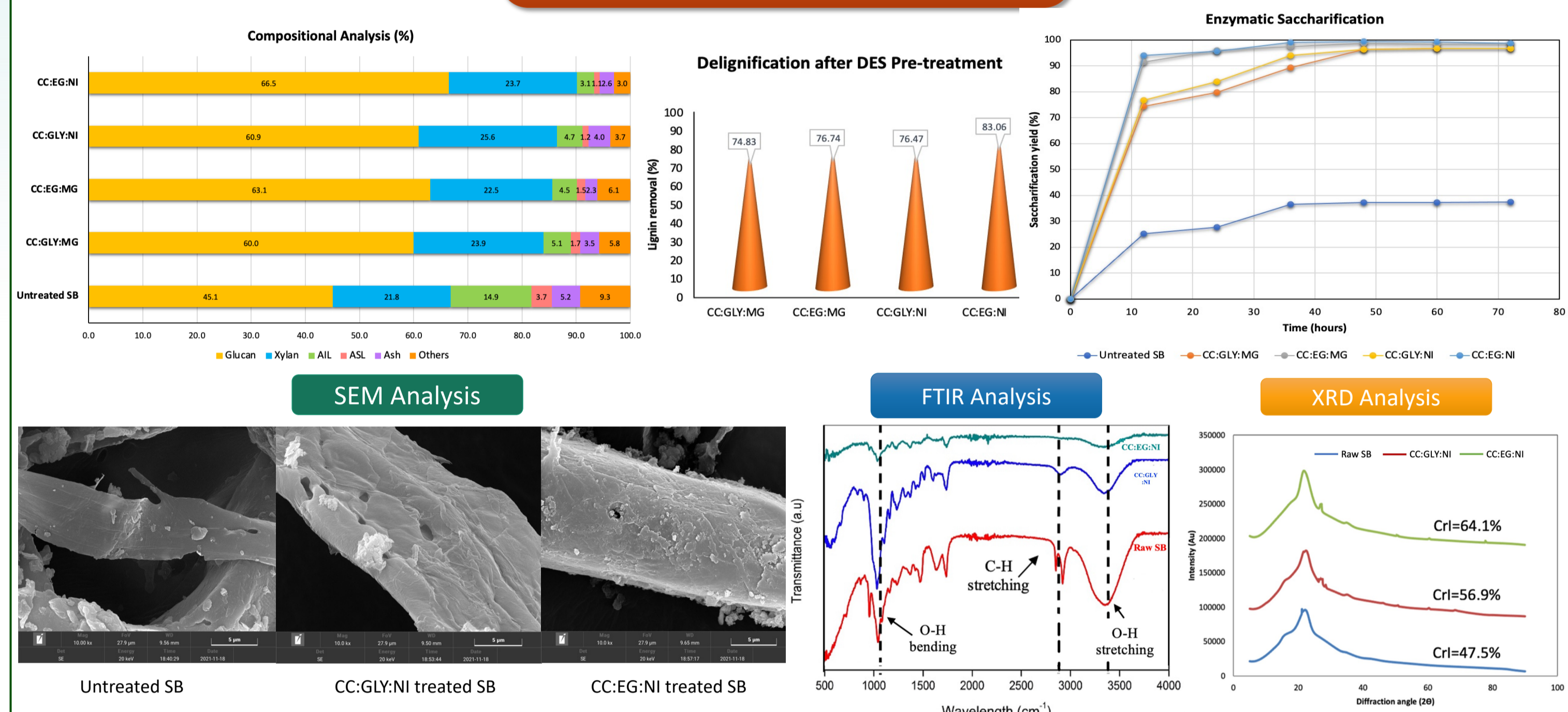
- Cellulase enzyme (
- Enzyme Loading: 10 FPU/g SB
- Conditions: 50 °C, 24 h

#### 3. Fermentation

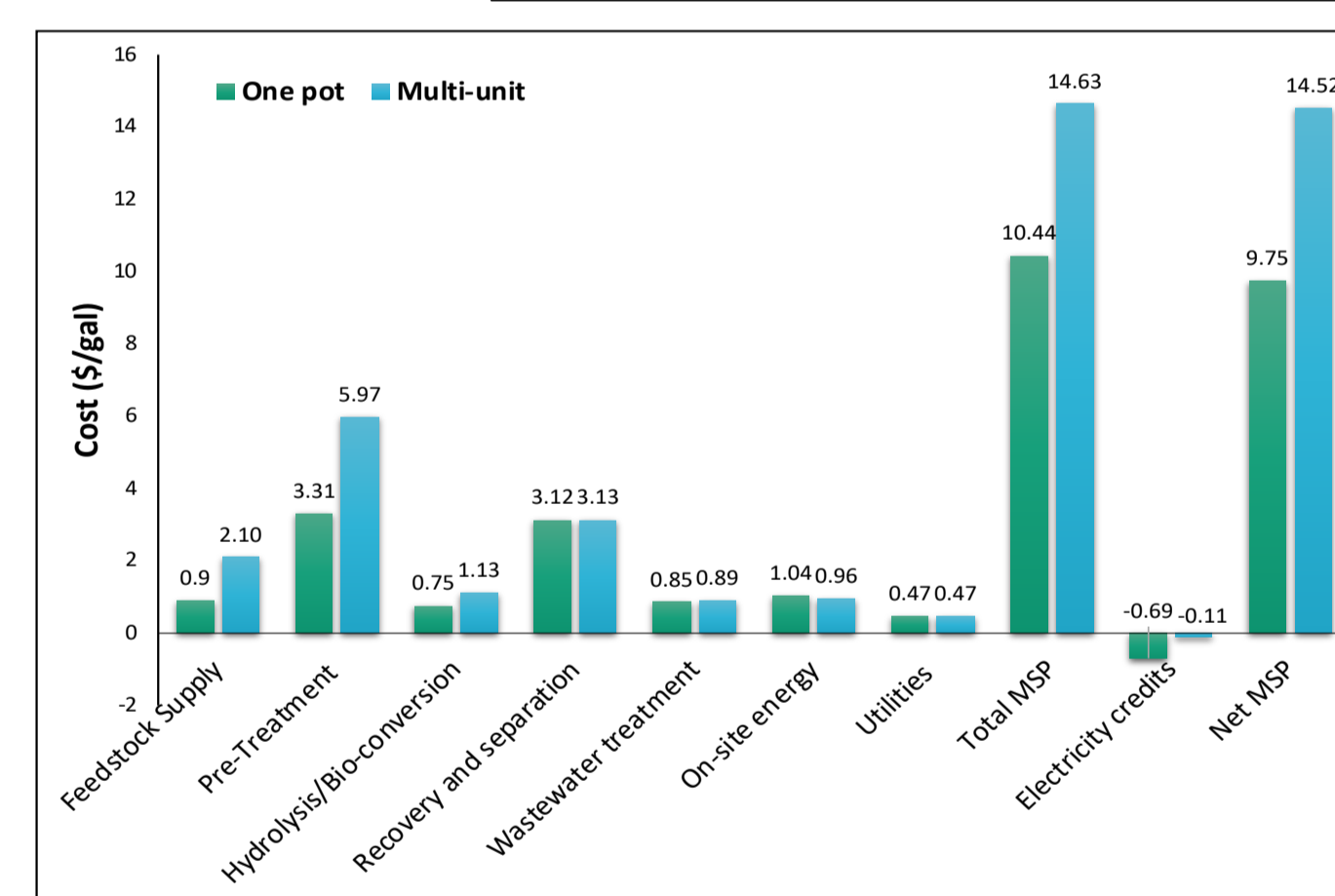
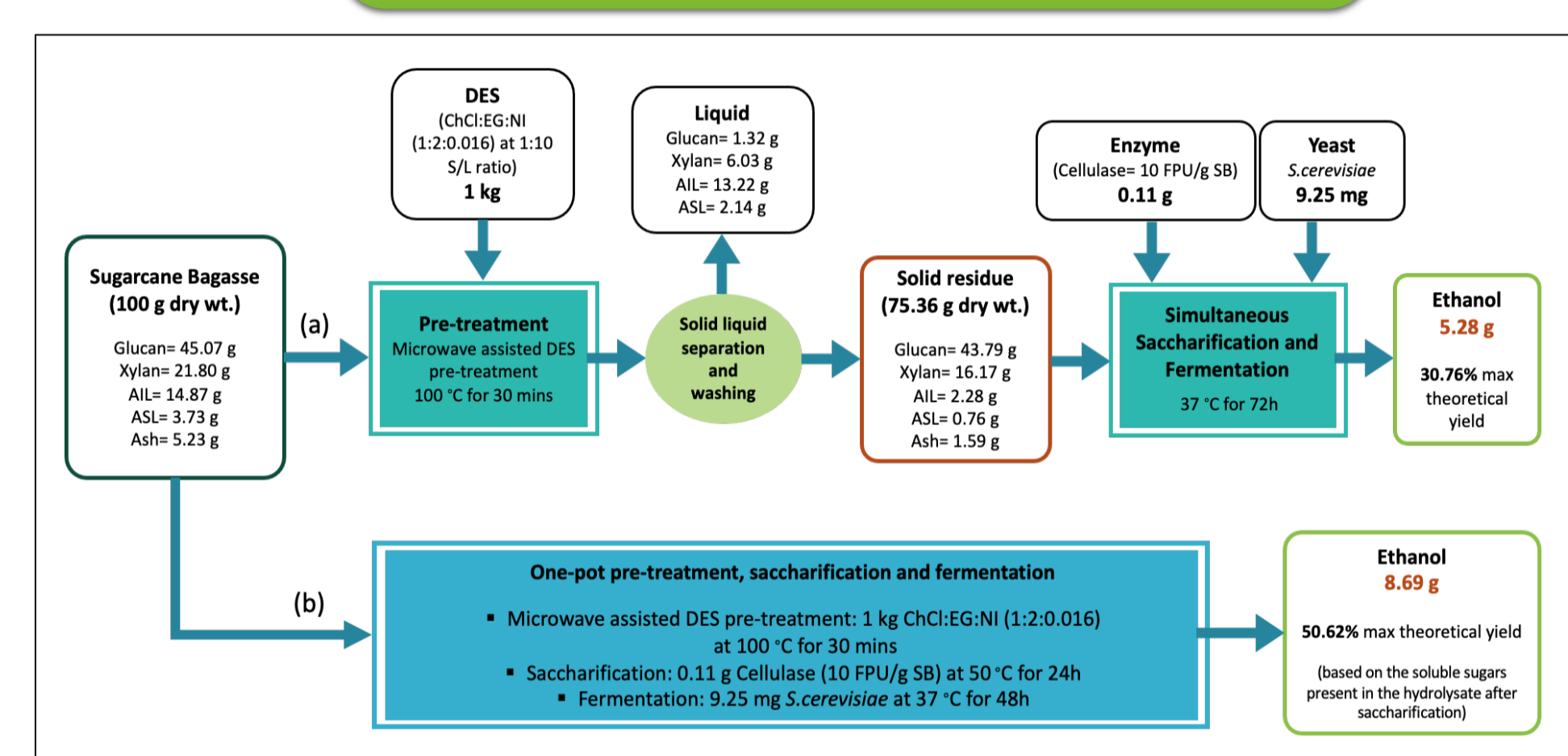
- Yeast (*Saccharomyces cerevisiae*,  $OD_{660} \sim 1.5 - 2.0$ ; cell concentration-  $10^8$  cells/mL)
- Inoculum: Hydrolysate::1:10
- Conditions: 37 °C, 48 h

## RESULTS AND DISCUSSION

### Biomass Characterization

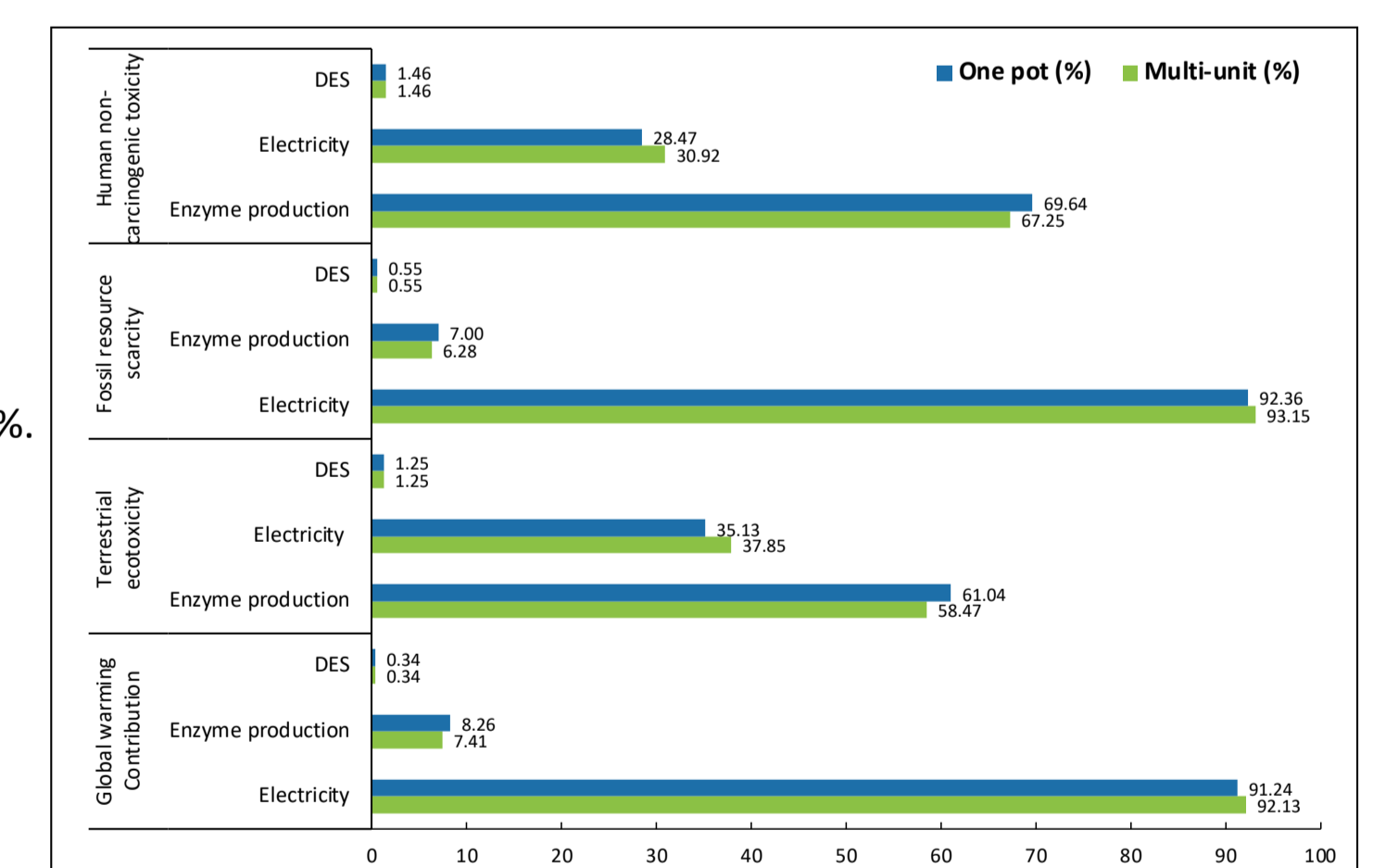


### One Pot Bioethanol Production



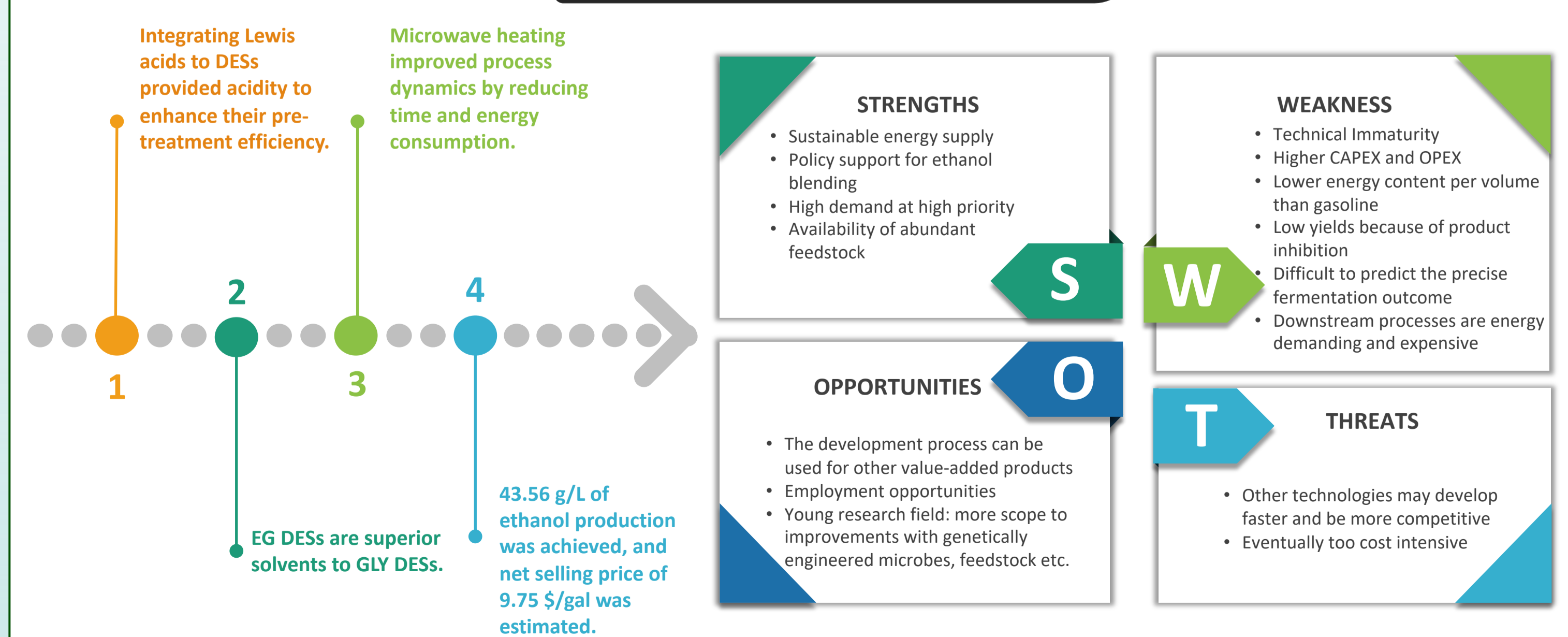
- Equipment cost data was taken from NREL technical report, 2011 and was adjusted for year 2022 using chemical engineering plant cost index.
- Cost calculation done by the method proposed by Sinnott and Towler.

Minimum Ethanol Selling Price (MESP) =  
Annual capital cost investment +  
Annual operating cost + cost of lignocellulosic feedstock  
Annual ethanol flow rate



- Open LCA with *ecoinvent 3.8* database
- Impact assessment method: *ReCiPe 2016*.
- Electricity consumption (70-93%), enzyme production (7-36%), DES ~1%.
- The impacts can be reduced by:
  - Changing the electricity mix.
  - Using engineered microbes can produce enzyme *in-situ* and co-utilize xlyose
  - Further process optimization and intensification

## CONCLUSION



## ACKNOWLEDGMENT

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